QUALITY OF THE STRUCTURE OF ASH BODIES BASED ON DIFFERENT TYPES OF ASH

KVALITETA STRUKTURE TELESA IZ PEPELA NA OSNOVI RAZLIČNIH VRST PEPELA

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Artificial aggregates based on the self-firing process are often produced with an outdated technology without innovations and research. The knowledge of the production of ceramic materials is useful, but fly ash is quite a heterogeneous material influenced by the thermal processes occurring during the production; therefore, this problem has to be solved. The aim of the research work was to evaluate the influence of the character of fly ash on the formation, structure and properties of a sintered fly-ash body using laboratory firings. The main difference as regards the behavior is between the fly ash originating from high temperature and the one originating from fluidized-bed combustion. While the first type of ash contains mainly mullite and other high-temperature minerals, the fluidized-bed-combustion ash contains mainly anhydrite and free lime. These increase, for fly-ash body. The content of Fe_2O_3 and its modifications and the proportion of SiO_2 in the amorphous phase or mullite are important parameters for evaluating various types of high-temperature combustion fly ashes. The content of Fe_2O_3 together with carbon finally works as a very effective fluxing agent. Thus, the surface of a specimen was sintered and the swelling was considerable due to the product gases of CO and CO₂. A higher proportion of SiO₂ contained in the amorphous phase increases the strength and the quality of a fly-ash body. A higher proportion of SiO₂ in the crystal phase requires a higher amount of heat for obtaining a solid structure.

Keywords: artificial aggregate, bottom ash, fly ash, FBC ash, sintering, clinkering

Umetna telesa, ki temeljijo na procesu zgorevanja, se pogosto izdelujejo po zaostali tehnologiji, brez inovacij in raziskav. Poznanje izdelave keramičnih materialov je koristno, vendar pa je leteči pepel zelo heterogen material, na katerega vplivajo toplotni procesi med proizvodnjo, zato je ta problem potrebno rešiti. Namen te preiskave je bil oceniti vpliv značilnosti letečega pepela za nastanek, strukturo in lastnosti teles iz sintranega letečega pepela za laboratorijskim žganjem. Glavna razlika glede na vedenje je med letečim pepelom, ki izvira iz visokih temperatur in tistim, ki izvira iz zgorevanja v zvrtinčeni plasti. Medtem ko prva vrsta pepela vsebuje pretežno mulit in druge visokotemperaturne minerale, vsebuje pepel iz zgorevanja v zvrtinčeni plasti predvsem anhidrit in prosto apno. To na primer poveča manipulacijsko trdnost mešanice letečega pepela, vendar poveča tudi količino mešalne vode in oslabi telo iz sintranega letečega pepela. Vsebnost Fe₂O₃ in njegovih modifikacij ter razmerja SiO₂ v amorfni fazi ali mulitu sta pomembna parametra pri oceni različnih vrst visokotemperaturnih letečih pepelov. Vsebnost Fe₂O₃ skupaj z ogljikom deluje kot zelo učinkovito talilo. Površina vzorcev je bila sintrana in pojavilo se je občutno nabrekanje zaradi nastajanja plinov CO in CO₂. Večji delež vsebnost SiO₂ v amorfni fazi je povečala trdnost in kvaliteto telesa iz letečega pepela. Večja vsebnost SiO₂ v kristalni fazi povzroča potrebo po večji količini toplote za pridobivanje trdne strukture.

Ključne besede: umetno telo, pepel, leteči pepel, FBC-pepel, sintranje, negorljiv ostanek

1 INTRODUCTION

Even after its previous treatment, a big part of the produced fly ash is still stored at a storing place and the cost for its liquidation is still considerable.¹ Generally, the volume of suitable fly-ash types produced in our country highly exceedes the possibilities of its processing in the building industry.²

In the first period of realisation our building industry is able to use suitably sintered artificial aggregates in the volume of $300-400 \cdot 10^3$ m³ annually.³ After its application has been generally accepted in the building industry this volume may continually increase. A former experience confirmed this expectation when the complete production of the Dětmarovice agglomeration factory (the Corson technology) was troublefree and used mostly in the North Moravia region. Considering the limited knowledge in this field, the operation and optimisation of this technology were very expensive and fly ash found its place in the traditional technologies of concrete production.⁴⁻⁶

The European and global trends in the new-technology development in the building industry require a production of high-quality light artificial aggregates, and its operation is increasing in the advanced countries.^{7,8}

In Central and Eastern Europe, only Poland reacted to this trend by constructing a factory for the artificialaggregate production using the sintered fly ash in Gdansk. The factory is equipped with licensed process equipment from Lytag, UK. However, the technology of this production process is even older than the Corson technology.⁹

The production technology for obtaining artificial aggregates by burning frequently uses the original format

of high-quality black-coal fly ash containing the optimum amount of unburned residues, burned with an external heat source and without the necessary correction of the fuel or the aggregate. Globally, there is no competition within this field and thus the involved companies do not commit to development and innovations. On that ground the procedures of obtaining artificial aggregates from sintered fly ash are relatively poorly explored and only a minimum scientific work is dedicated to the process of producing fly-ash bodies by burning. Therefore, if we consider the possibility of restoring the production in inland conditions it is necessary not only to innovate the existing technology but also, in particular, to commit to the study of reaction processes in the solid phase and the creation of fly-ash aggregates.

2 EXPERIMENTAL WORK

At the beginning the experimental activity was focused on the characterization of the selected types of ashes, representing the current production plants of the Czech Republic. We selected five samples of fly ashes obtained with the combustion of coal at temperatures of 1200-1600 °C, with its desulphurization taking place after the separation by means of a lime solution. We had one sample of black-coal fly ash (FFA), three samples of brown-coal fly ashes from the silos of three different power plants (FA1, FA2, FA3s) and one sample of a finer fly ash (2nd electrostatic separator) from the third plant (FA3f). There were also two samples from a power plant with the fluidized-bed combustion (FBC) of brown coal. This type of combustion takes place at the temperatures of around 850 °C and desulphurization is carried out in the furnace. One sample was from the electrostatic separator (FBC FA) and one from the bottom of the furnace (FBC BA).

The following physico-mechanical and physico-chemical parameters were selected: the loss on ignition (ČSN 72 0103) showing unburned residues, the bulk density (ČSN 72 2071), the specific surface area and remains on the sieve of 0.090 mm (CSN 72 2072-6). The chemical and mineralogical analyses were also carried out. In order to monitor the behavior of the samples during the firing process, a special type of annealing microscopy was chosen. Cylinders of 3 mm in cross-section were made. They were placed into an annealing chamber equipped with a camera and backlight to capture the changes in the sample cross-sections during the annealing (10 °C/min, max. 1600 °C). The current temperature and the changes to the sample cross-sectional areas were primarily recorded.

The influence of fly ash on the physico-mechanical properties of a fired ceramic body was determined on the samples fired in a muffle kiln. Fly ash was mixed with water to reach the limit of fluidity. We made samples with the size of 20 mm \times 20 mm \times 100 mm that were, next day, dried at 60 °C for 2 h and then fired in the muffle kiln. The firing was characterized by the initial temperature of 25 °C, a rate of firing the muffle kiln of 300 °C/h and an isothermal dwell time at 1150 °C of 10 min. After the firing and natural cooling down, the specimens were taken out of the kiln and placed in a desiccator. After a thermal stabilization, their volume weight (ČSN EN 1015-10 and ČSN EN 1015-6), the compressive strength (ČSN EN 14617-15) and the water-absorbing capacity (ČSN EN 1097-6) were determined.

3 RESULTS AND DISCUSSION

First of all there are the results characterizing the ashes tested. In **Table 1** you can see the results determining the physico-mechanical and physico-chemical parameters and the results of the chemical analysis.

The analysis of the unburned residues of the tested fly ash shows that apart from fly ash FFA, all the samples fulfill the requirements of the standard (CSN 72 2072-6, 2013) for the maximum loss on ignition of 15 %. Therefore, this fly ash was used as the fuel (FuelFlyAsh) in this work. The determination of the bulk density shows that the fly ash from high-temperature combustion reaches higher values than the fly ash from fluidized-bed combustion. All the values of the high-temperature fly-ash samples and the bottom ash fulfill the requirements of the standard (CSN 72 2072-6, 2013) for the minimum value of 800 kg m⁻³. The low values of the bulk density of samples FFA and FBC show a porous structure of the coal grains.

 Table 1: Physico-mechanical and physico-chemical parameters of the tested ashes

 Tabela 1: Fizikalno-mehanski in fizikalno-kemijski parametri preizkušanih pepelov

	Loss on ignition	Bulk density	Specific surface	Remains on the sieve, 0.090 mm	Chemical composition (%)					
	%	kg m ⁻³	m ² kg ⁻¹	%	SiO ₂	Al ₂ O ₃	Fe ₂ O ₃	SO ₃	CaO	
FA1	1.19	990	329	37	47.7	28.2	5.6	0.1	1.1	
FA2	1.07	1110	299	33	54.6	29.5	5.5	0.1	1.8	
FA3s	2.39	1010	234	51	50.0	23.4	14.5	0.3	3.4	
FA3f	1.97	940	262	9	48.3	22.8	16.6	0.5	3.7	
FFA	27.12	830	398	33	36.0	16.4	8.9	0.4	5.0	
FBCFA	2.08	810	353	32	42.7	26.8	5.1	3.0	10.2	
FBCBA	4.23	1210	33	88	42.3	26.7	5.2	3.1	10.3	

	Quartz	Mullite	Hematite	Anortite	Lime	Calcite	Anhydrite	Amorphous
	SiO ₂	Al ₆ Si ₂ O ₁₃	Fe_2O_3	CaAl ₂ Si ₂ O ₈	CaO	CaCO ₃	CaSO ₄	phase
Melting point (°C)	1470	1810	1350	1550	2613	825	1400	-
FA1	7.0	39.3	1.2	2.7	_	_	_	39.5
FA2	7.8	32.3	_	-	_	_	_	58.1
FA3s	7.1	18.2	3.3	8.7	_	-	-	55.6
FA3f	6.8	17.3	3.5	8.5	_	_	_	58.4
FFA	13.0	12.4	2.0	4.2	0.8	0.5	-	57.5
FBCFA	9.5	_	3.3	_	3.2	3.8	5.7	63.8
FBCBA	8.8	_	3.4	_	3.4	3.6	5.9	58.9

 Table 2: Results of the mineralogical analysis of the tested ashes

 Tabela 2: Rezultati mineraloških analiz preizkušanih pepelov

In most cases, the specific surface corresponds to the results of the granulometry of fly ash. Higher values show a better quality of the reaction in the solid phase and the formation of a stronger structure of the aggregate.

The results of the chemical analysis show that hightemperature ashes usually achieve a higher content of SiO_2 . FA2 has the highest value. The FBC ash samples achieved higher contents of CaO and SO₃ as the sulphate sulphur. This helps us obtain higher strengths of fresh samples.

Because of the SO₃ exceeding limits (CSN 72 2072-6, max. 3 %) it will be necessary to install desulphurization of the production line in the future. The content of Fe₂O₃ is an important parameter and it acts as a fluxing agent during the firing, enclosing the surface of an aggregate. Consequently, the fumes cannot leave freely and a reductive core is produced. The grains show a more considerable porosity under the surface.¹⁰ This problem can be assumed during the production of the aggregate based on fly ash FA3.

As you can see in **Table 2**, FA1 has the highest percentage of mullite and a lower content of the amorphous phase in comparison with FA2. The mineralogical analysis further confirms that FA3 contains more minerals with a lower melting point and a low content of mullite. Fluidized-bed ashes have almost no content of mullite. The FBC ashes achieve higher contents of the minerals based on CaO that shorten the sintering interval and decrease the melting point of the material.

In **Figure 1** you can see the results of the annealing microscopy. Specifically, there is a dependence of the area of the sample on the firing temperature. The samples are stable up to 1150 °C. The samples of fly ashes went through a certain sintering phase, followed by the swelling caused by the generated gases. Higher contents of Fe₂O₃ in FA3s and FA3f, together with the carbon, cause a reduction in FeO, which then functions as a highly active flux.¹⁰ This leads to the sintering of the sample surface and a subsequent significant swelling caused by the generated gases of CO and CO₂. As you can see, the finer ash of FA3f achieves the highest swelling (180 %). This is one of the reasons why the rate of firing the muffle kiln of 300 °C/h was chosen. A higher firing rate can create samples with unsuitable shapes. At the melting point, the melting starts. The annealing of fluid fly ash is significantly affected by the presence of CaSO₄, CaCO₃ or CaO alone. The first two minerals show their degradation during the firing and the subsequent percentage of CaO significantly lowers the melting point of the other minerals.

Figure 2 shows the results of the shrinkage; Figure 3 shows the compressive strength and Figure 4 the water absorption of the fired samples.

The highest shrinkage was measured for the samples based on the FBC ashes, exhibiting a higher porosity,



Figure 1: Changes to the sample cross-sectional area during annealing Slika 1: Spremembe prečnega prereza vzorcev med žarjenjem

Materiali in tehnologije / Materials and technology 49 (2015) 4, 601-605



Figure 2: Shrinkage of the fired samples **Slika 2:** Skrček žganih vzorcev

V. CERNY: QUALITY OF THE STRUCTURE OF ASH BODIES BASED ON DIFFERENT TYPES OF ASH



Slika 3: Tlačna trdnost žganih vzorcev

and a decomposition of the CaO products caused a disintegration of the structure. This is the reason why a low compressive strength was also measured. An addition of high-temperature ash (FBC FA + 24 % FFA; FBC BA + 16 % FFA) increased the strength only on a small scale.

A high shrinkage was also measured for the sample based on FA3f, which had the highest content of the particles under 0.009 mm. Due to a higher content of Fe_2O_3 the highest compressive strength was measured. The shrinkage and closed porosity caused a very low water absorption. The addition of FFA as a fuel caused a high swelling (negative values for the shrinkage) and the samples then were not useable for the measurement of the physico-mechanical parameters.

The fly ashes from the silo (FA1, FA2, FA3s) had stable structures and achieved a lower shrinkage. A higher content of the amorphous phase and a low content of mullite caused higher compressive strengths of the FA2 samples. An addition of FFA (27 %) in combination with FA2 caused a structural weakening.

As you can see in **Figure 4** high-temperature ashes achieved lower values of water absorption in comparison with the FBC ashes.

In Figures 5 and 6 you can see the differences between the samples based on the fly ashes with lower and higher contents of Fe_2O_3 . Figure 5 shows the closed



Figure 5: Closed structure of the FA2 sample Slika 5: Zaprta struktura vzorca FA2

homogeneous structure of FA2 and **Figure 6** shows the swollen core of the sample based on FA3s causing an enclosed surface.

4 CONCLUSIONS

When assessing the suitability of fly ash, the main difference can be seen between the high-temperature fly ash and the FBC ash. The first type mainly contains high-temperature minerals like mullite. The FBC ashes mainly contain anhydrite and free lime, which increase the manipulation strength of fresh samples, but they also increase the amount of mixing water, weakening the sintered fly-ash body and creating open porosity. The FBC ashes are not very suitable for sintered aggregates.

When assessing the influence of the quality of high-temperature fly ash on the quality of an ash body, the main parameters are the loss on ignition, the remains on the sieve of 0.009 mm, the contents of SiO₂, Fe₂O₃, quartz, mullite and the amorphous phase. The maximum loss on ignition is 8 %. Higher values classify the ash as a fuel. Finer ashes create more solid structures with small pores at lower temperatures. A higher content of SiO₂ in the amorphous phase ensures a higher strength.







Figure 6: Swollen surface of the FA3s sample **Slika 6:** Napihnjena površina vzorca FA3s

Materiali in tehnologije / Materials and technology 49 (2015) 4, 601-605

A higher content of mullite needs a higher temperature for creating a solid structure. The content of Fe_2O_3 together with carbon finally works as a very effective fluxing agent. Thus, the surface of a specimen is sintered faster and the firing product gases of CO and CO₂ can cause a considerable swelling.

Further work will focus on the influence of a faster temperature rise during the annealing microscopy on the area change and the impact of increasing the firing temperature to $1200 \degree C$ on the physico-mechanical parameters and mineralogical changes.

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